

Water Softening Improvements

at the City of Harrison Water Treatment Plant

2024 CSEAO Winter Conference

December 6, 2024



System Overview

- Source: Groundwater
- Supply: Seven production wells
 - Ohio wellfield (4 wells)
 - Indiana wellfield (3 wells)
 - Firm capacity 4.46 MGD
Total capacity 5.76 MGD
- Previous Water Treatment Plant Operations:
 - Did not include softening
 - Iron/Manganese removal by chemical oxidation and pressure filtration
 - 2.93 MGD treatment capacity



Project Need

Hardness (mg/L as CaCO ₃)	Description	Effect(s)
0 – 50	Extremely soft	Corrosive. Skin feels slimy when wet.
50 – 100	Very soft	Can be corrosive.
100 – 150	Soft to moderately hard	Often acceptable to most users.
150 – 300	Hard	Staining, scaling of plumbing fixtures.
> 300	Very hard	Scum in the bath and shower, scaling on cookware and in water heaters/boilers, and requires more laundry detergent.

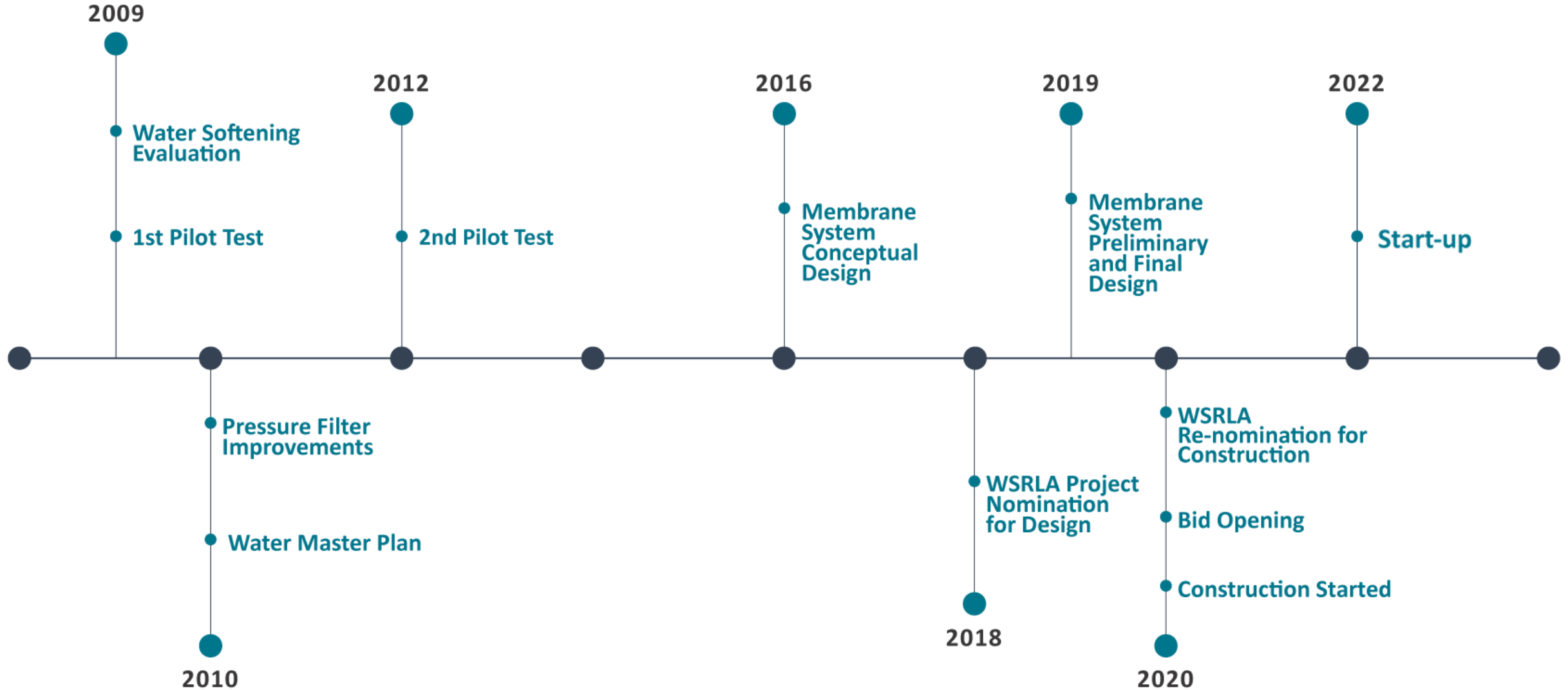
Harrison water hardness is 320–490 mg/L
“very hard”

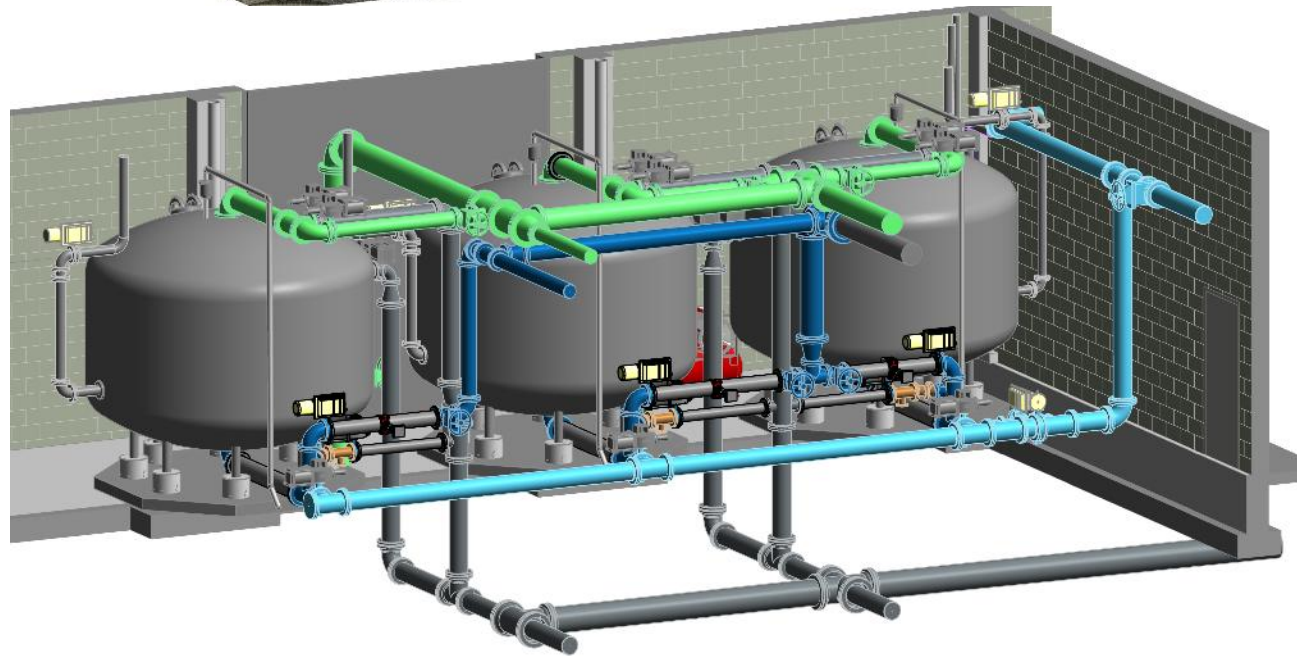
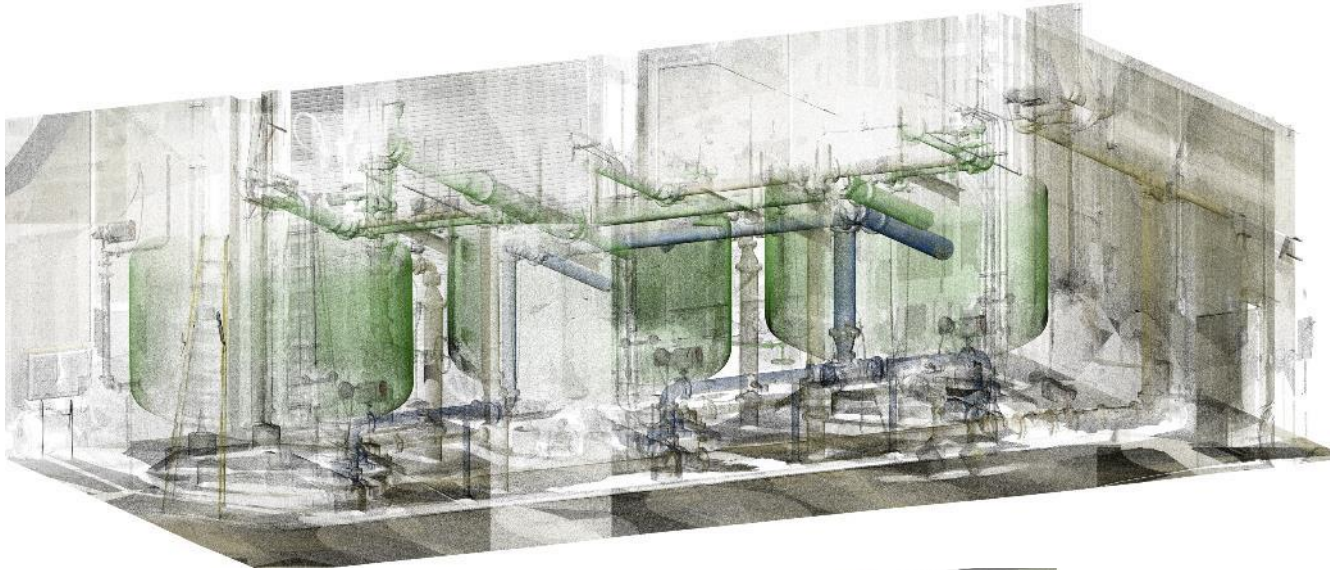
Hard Water Consequences

- Why add membrane softening?
 - Causes scum in bath/shower and fixtures
 - Causes scaling on cookware and in water heaters/boilers
 - Complexes with soap, reducing laundering effectiveness
 - Soap can't interact with dirt on clothing, forming undesirable precipitates



Project Timeline

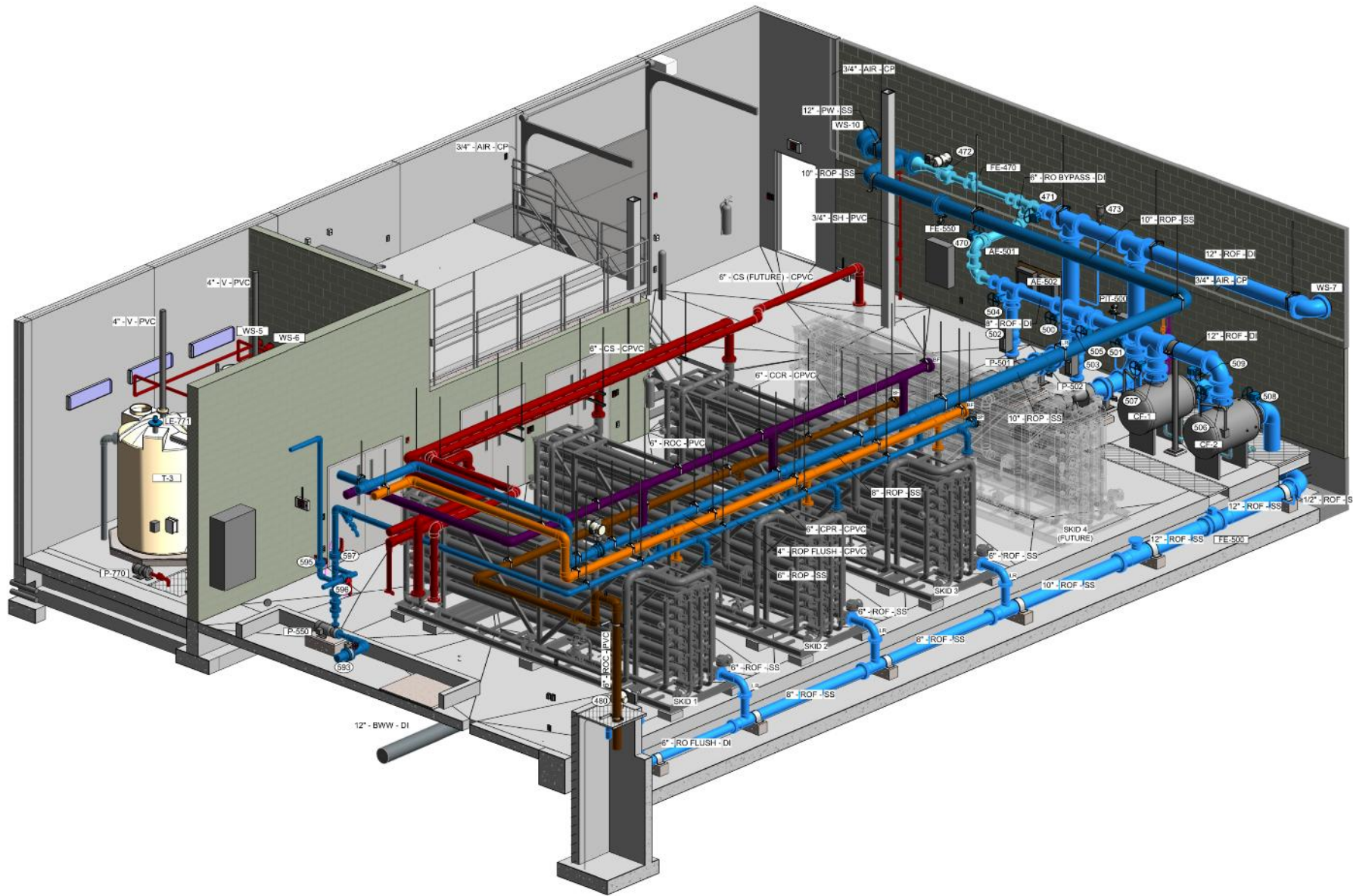




Creation of As-Built Model

*Laser Scanning
Scan-to-BIM*

40 scans of existing facility were performed

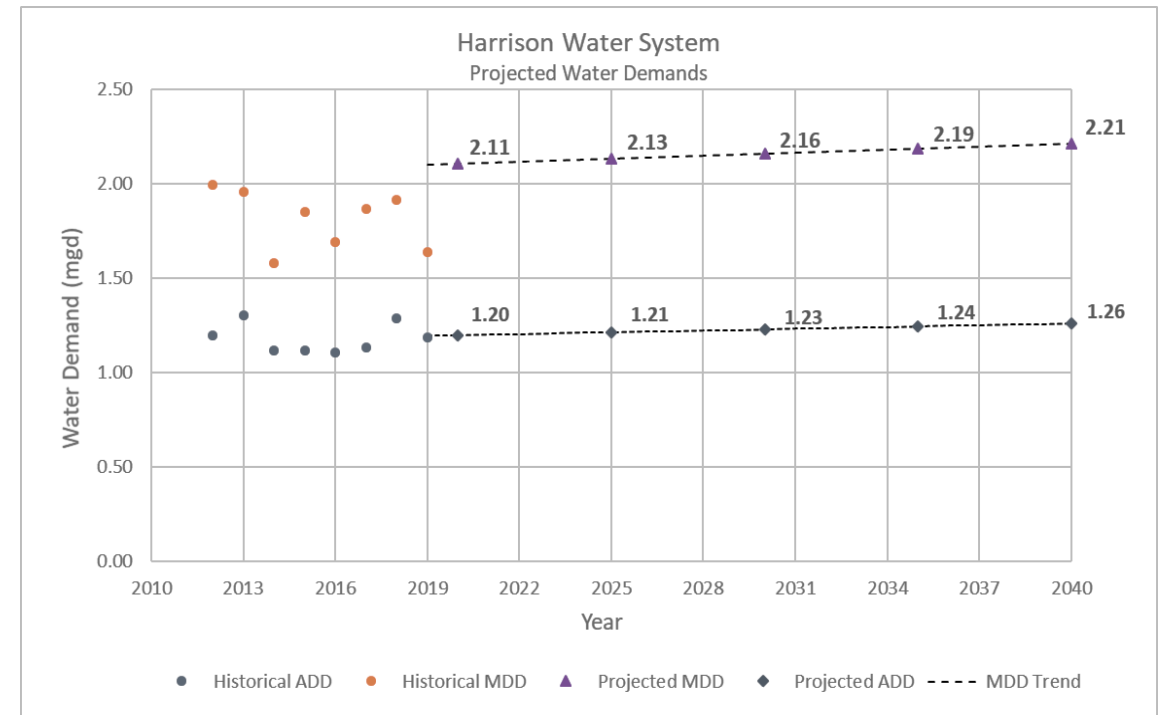


Building Addition Model

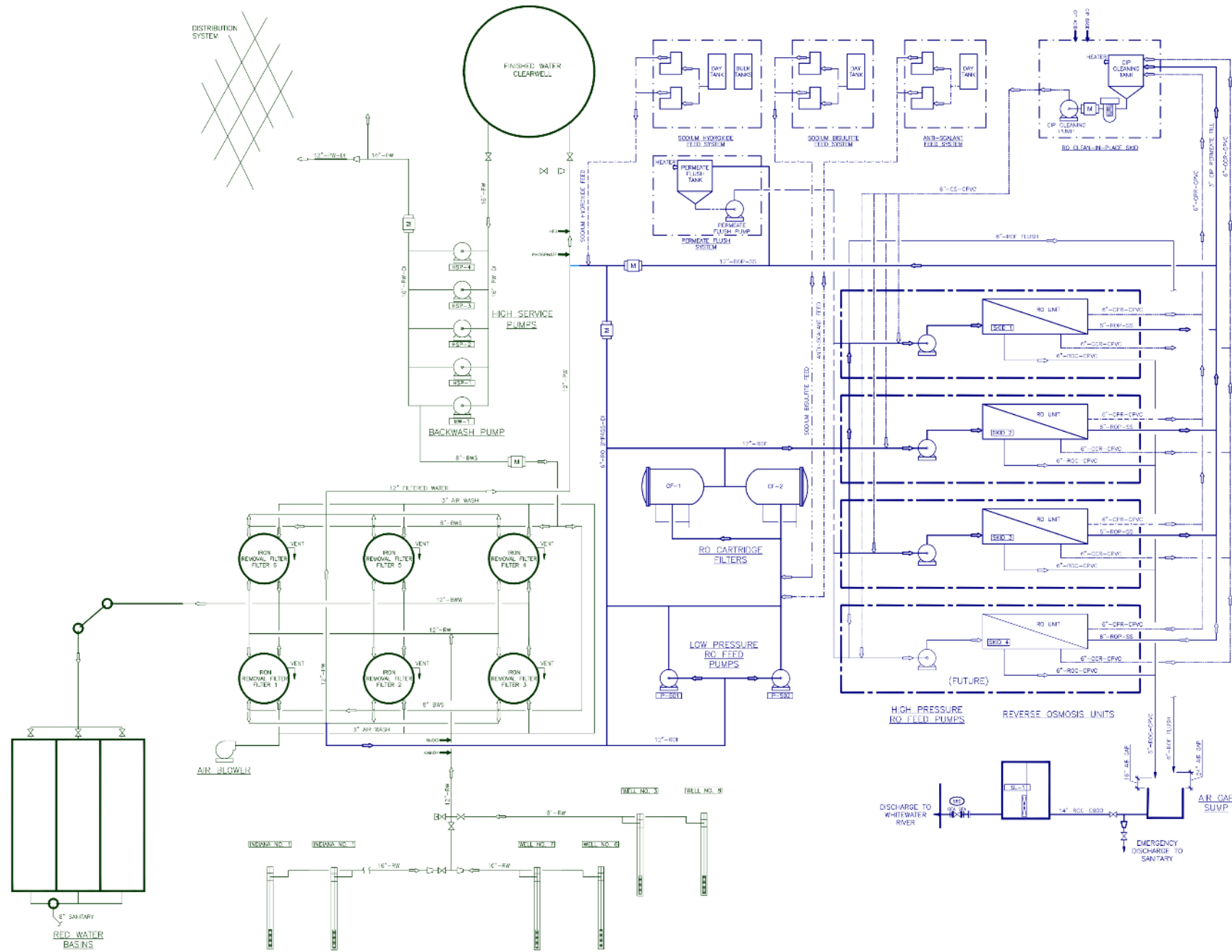
Autodesk Revit
BIM 360
Autodesk Navisworks

Treatment Basis of Design

- **Filtration**
 - 2.93 MGD at a filtration rate of 3.0 gpm/sf
- **Softening Capacity**
 - 2.4 MGD initially, 3.2 MGD future
- **Recovery Rates**
 - Membrane Recovery: 75–80%
 - Discharge to Whitewater River: 20-25%
- **Concentrate Volume**
 - Average Day: 300,000 gallons/day
 - Maximum Day: 530,000 gallons/day
- **Finished Water Goals**
 - Target Hardness between 120–140 mg/L as CaCO_3



Projected Water Demands



System Design

Pretreatment Improvements

- Valves and actuators upgraded
- Meters replaced
- Media replaced
- Controls upgraded
- Validation Steps
 - Filter run SDI profiles
 - Filter to waste SDI profiles



Existing filter piping, valves and actuators



Low Pressure RO Feed Pumps

- Boost filter effluent pressure
- Bypass control valve
- Cartridge filter headloss

Chemical Addition

- Antiscalant
- Sodium bisulfite
- Feed points at static mixer
- Fed prior to cartridge filters
- Continuous monitoring



Photo credit: Avista Technology — iron fouled membrane

Chemical Feed Room

- **Antiscalant and Sodium Bisulfite**
 - Converted Tote
 - Day Tank on Scale
 - Watson Marlow Qdos Pod
- **Sodium Hydroxide**
 - Two Bulk Tanks
 - Day Tank on Scale
 - Watson Marlow Qdos Pod





Cartridge Filters

- Lead/Standby – 100% duty
- Located off-skid
- Horizontal vs. vertical



Cartridge Filters

- Density Rating: 5 μm
- Max Loading Rate:
 - 3.5 gpm/10-inch
 - 1.7 gpm/10-inch (both online)
- Manufacturer:
 - Fil-Trek MP Series
- Filters: 118 each SOE
- O-rings: EPDM

Membrane Elements

- **Active Area:**
 - 400 sf/element
- **Feed Spacer:**
 - 34 mil
- **Listed Manufacturers:**
 - Dupont, FilmTec BW30XFRLE-400/34
 - Toray, Model TMG20D-400



Dupont FilmTec RO element

Initial Membrane Element Loading



Start of Day



Later That Day



RO Feed Flush

- Automated
 - Pre-flush when skid comes online
- Flushes non-optimum feed water
- Allows chemistry to stabilize



RO Skids

- Configuration:
 - 12:6 with 7 elements/vessel
- Max Overall Flux:
 - 12 gfd
- Design Recovery: 75-80%
 - 10/22: Started Up 75%
 - 6/23: Increased to 80%

High Pressure RO Feed Pump

- High Pressure RO Feed Pumps
 - Vary speed to maintain steady permeate flow
- Design Point
 - Maximum recovery
 - 5-year conditions
 - 20% fouling factor
 - Permeate header pressure
 - Concentrate header pressure





CIP System Criteria

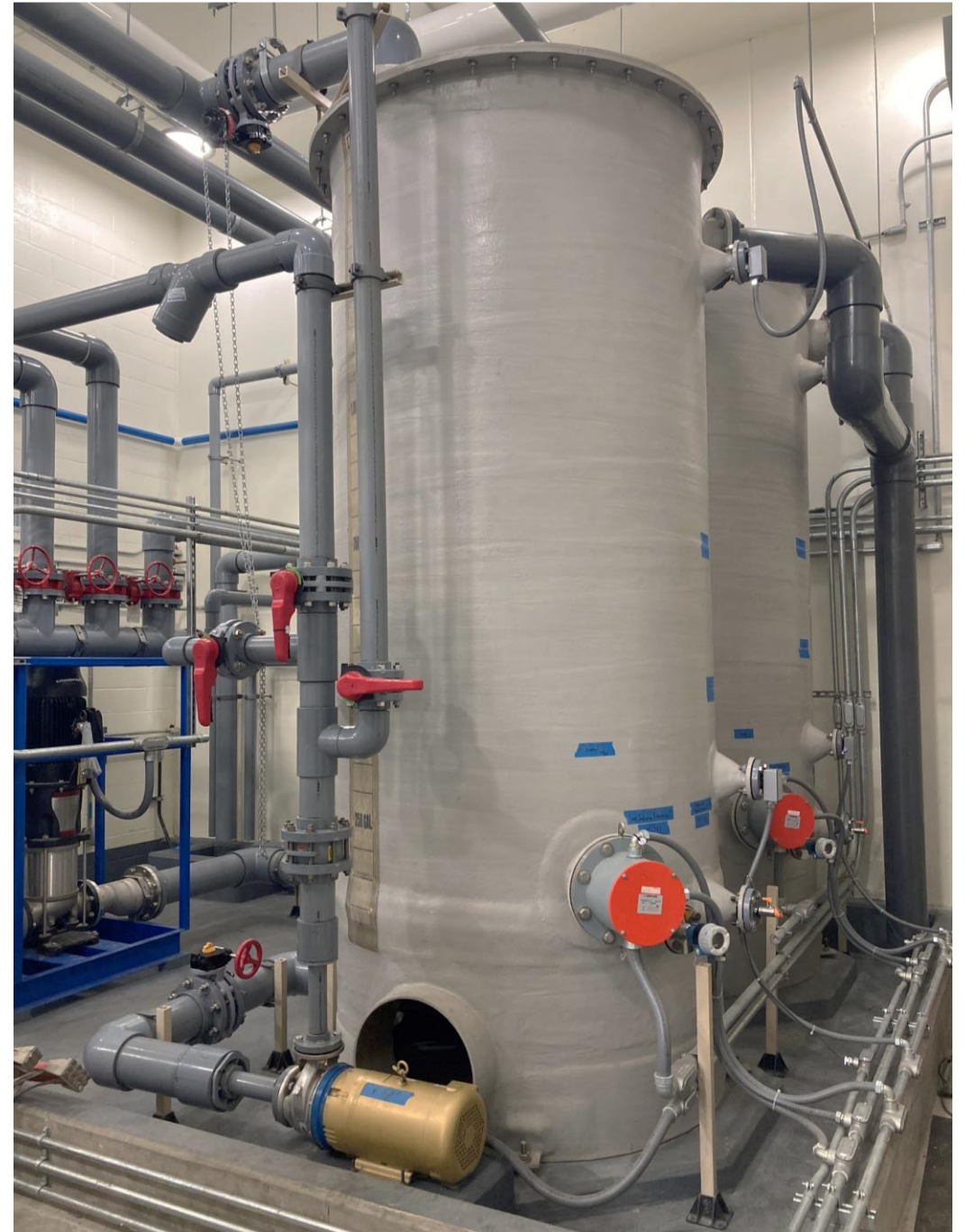
- Clean stages independently
- Right-size CIP pump w/ VFD
- Flexibility: liquid vs. powder
- Right-size CIP tank
- Dedicated CIP supply piping
- FRP tank
- CIP cartridge filter
- Double block and bleed



CIP Cleaning Chemical Room

Permeate Flush System

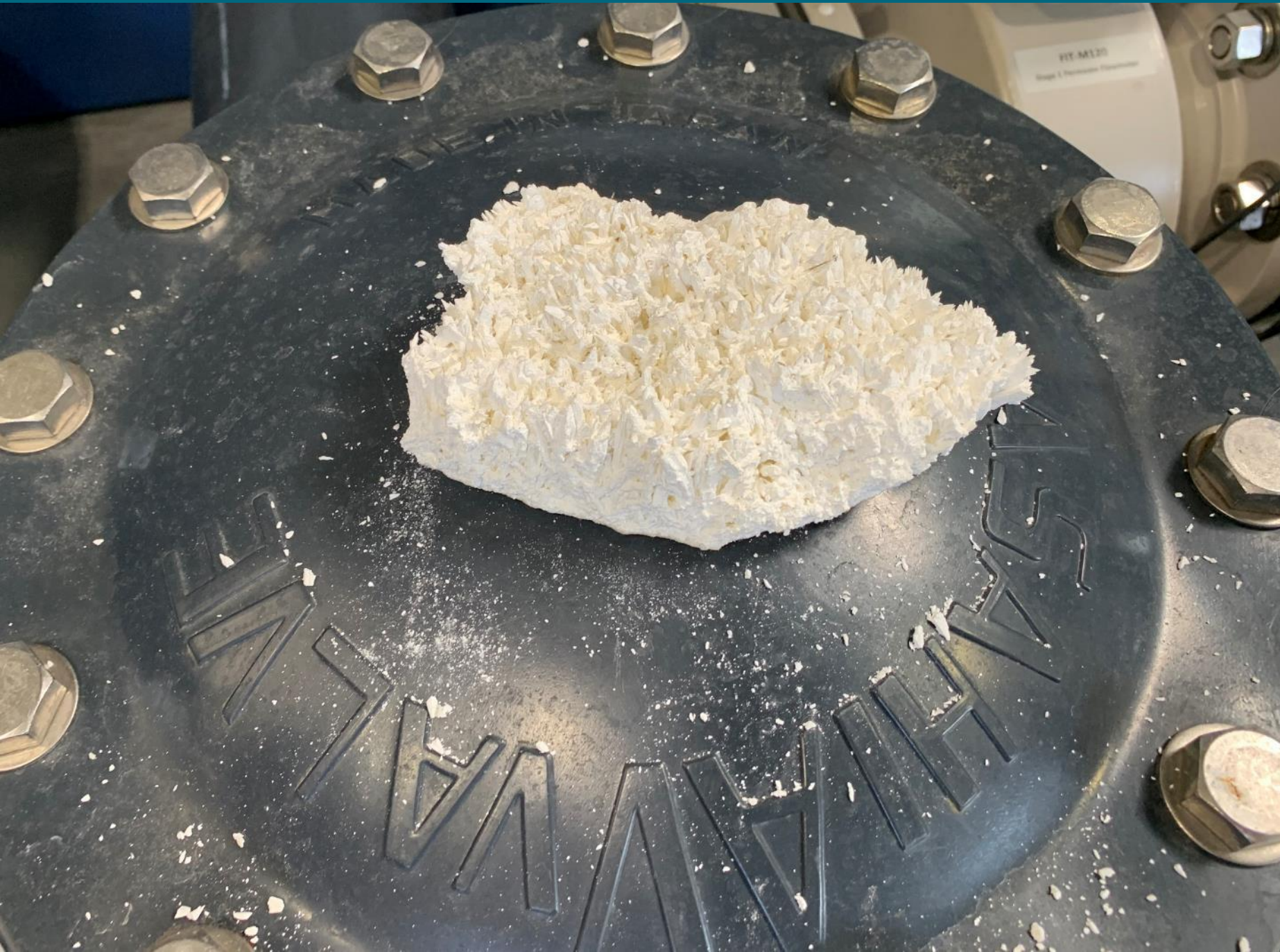
- Permeate Flush Tank
 - Exchange skid volume
- Permeate Flush Pump w/ VFD
 - 10 gpm/vessel at 30 psi
- Dual Function



Bid Evaluation

- **System Description**
 - Skid dimensions
 - Array configuration
 - Scope of supply
 - Element manufacturer & model
- **Performance Projections**
 - at 0, 3, and 5 years

APPENDIX B			
System Description Table			
Table B.1 RO/NF system(s)			
Description	Units of Measurement		Data
	If US Customary Units	If Metric Units	
MANUFACTURER	—	—	—
MODULE DESCRIPTION	—	—	—
Module model number	—	—	—
Type (RO, NF, or other)	—	—	—
Module dimensions:	—	—	—
Diameter or width (indicate which)	in.	mm	—
Length	in.	mm	—
Height, if applicable	in.	mm	—
Active membrane area, feed-side surface	ft ²	m ²	—
Membrane material (Examples: TFC, CA, CTA, and so on)	—	—	—
Second membrane material, if more than 1 type in system	—	—	—
If more than 1 membrane type, describe each type (i.e., first is anionic, etc.)	—	—	—
Configuration, select one or add description: flat plate, hollow fiber, spiral, tubular, or other (add description)	—	—	—
Geometry (horizontal or vertical)	—	—	—
Hydrophobic or hydrophilic?	—	—	—
Membrane charge (neutral, negative, or positive)	—	—	—
Molecular weight cutoff, nominal	dalton	dalton	—
Standard test conditions and performance	—	—	—
Feed concentration and solute	mg/L	mg/L	—
Feed pressure	psi	bar	—
Feed temperature	°F	°C	—
Feed pH	pH units	pH units	—
Recovery	percent	percent	—
Rejection	percent	percent	—
Permeate concentration, maximum	mg/L	mg/L	—
Permeate concentration, average	gpd	Lpd	—
Permeate flow, range	gpd	Lpd	—
Permeate flow, average	gpd	Lpd	—
NOTES: TFC = thin film composite CA = cellulose acetate CTA = cellulose triacetate			
(Table continued next page)			

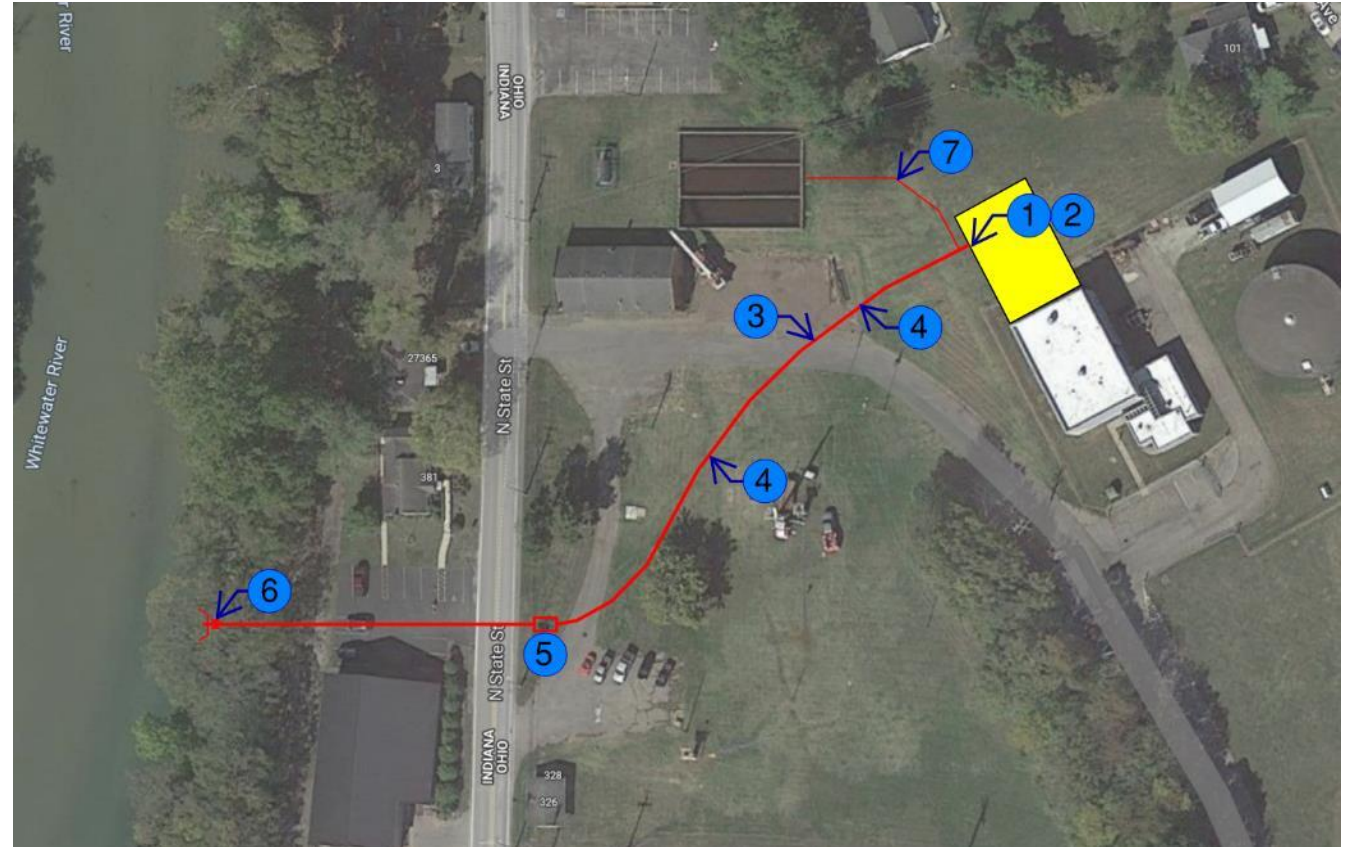


Concentrate Disposal Challenges

Wet Well = Scaling Pit
Long Pipe = Plugged Pipe

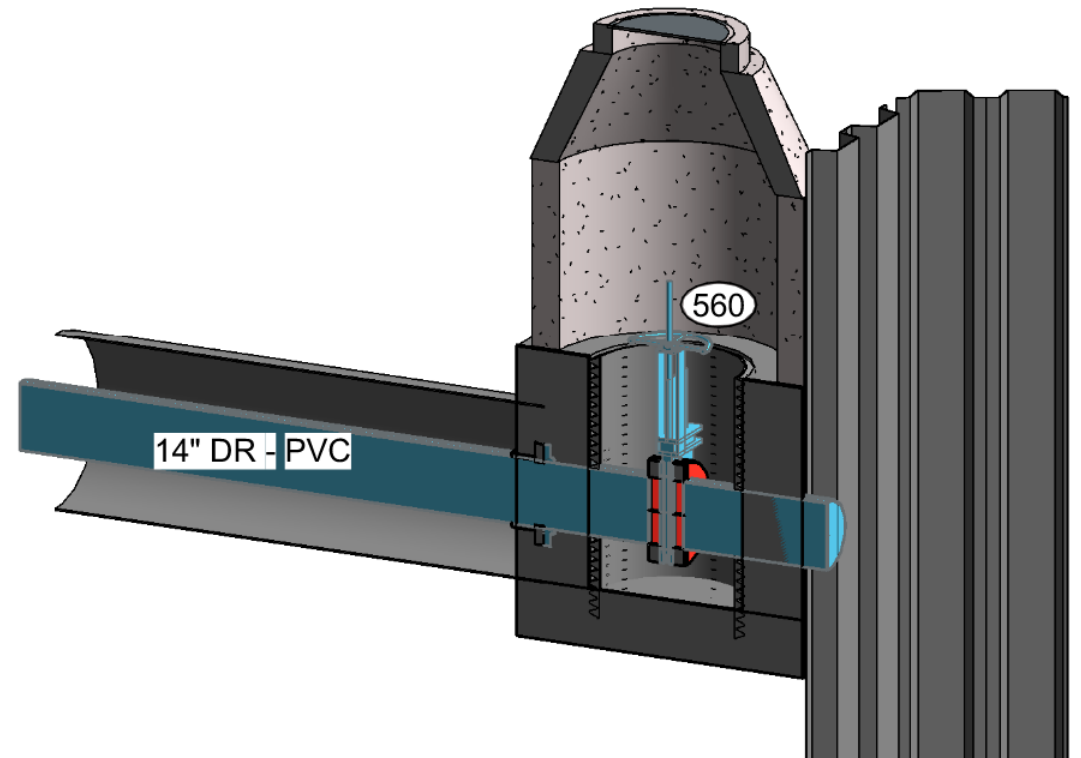
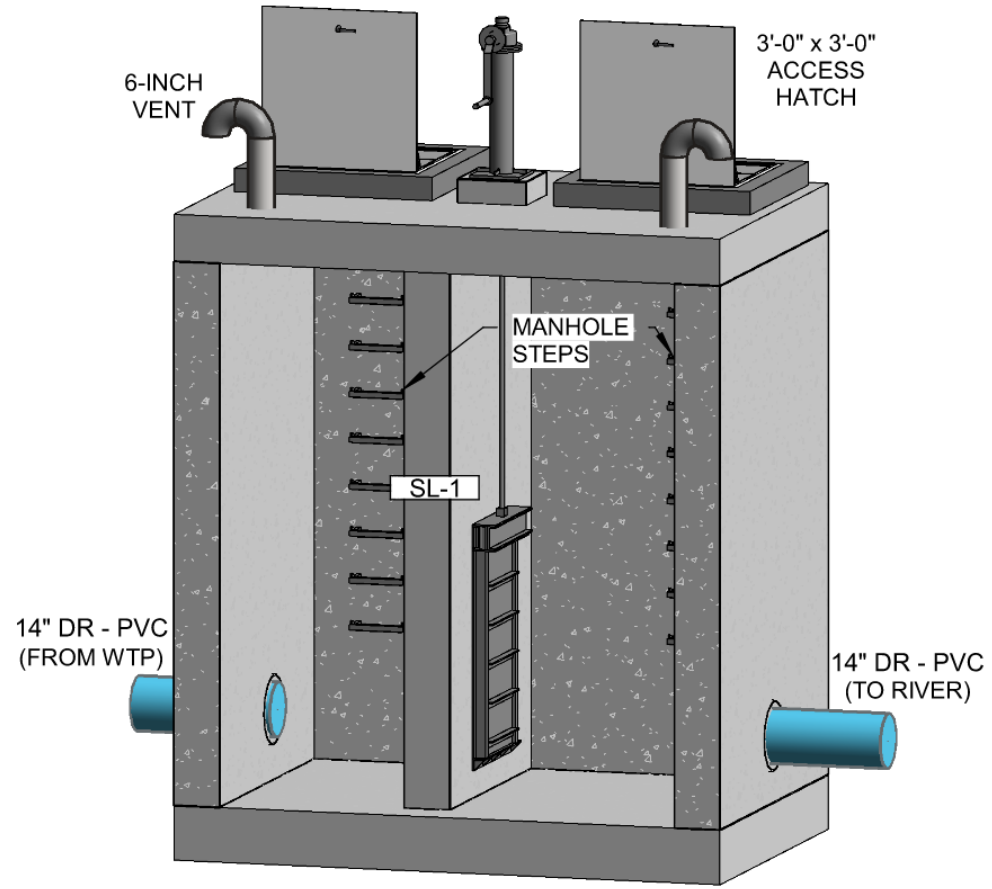
Concentrate Management

1. Air gap sump
2. RO feed flush
3. C900 pipe
4. Clean outs
5. Slide gate structure
6. Outfall knife gate
7. Emergency discharge to sanitary system



Concentrate disposal to Whitewater River

Whitewater River Outfall



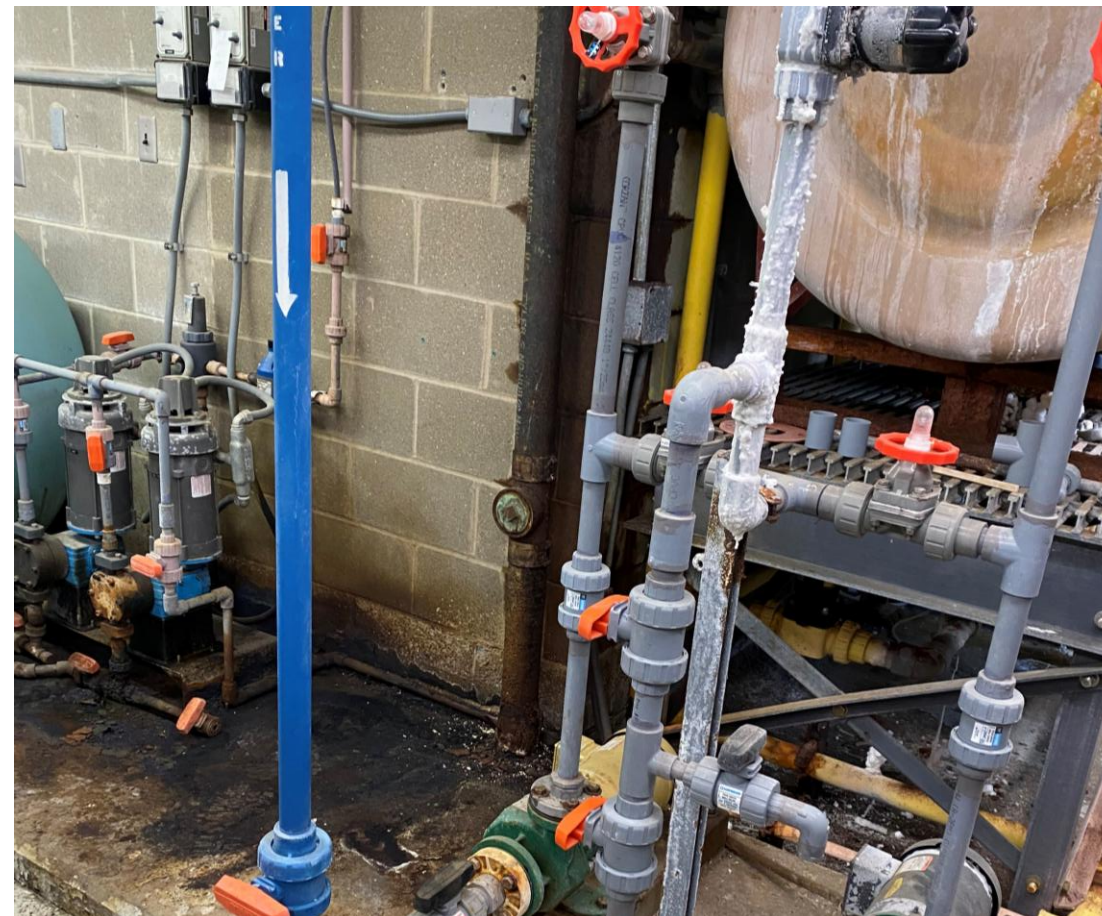


Outfall Headwall

Whitewater River Outfall



Chemical Room Improvements





Slab/Curb Replacement



Chemical Room Improvements



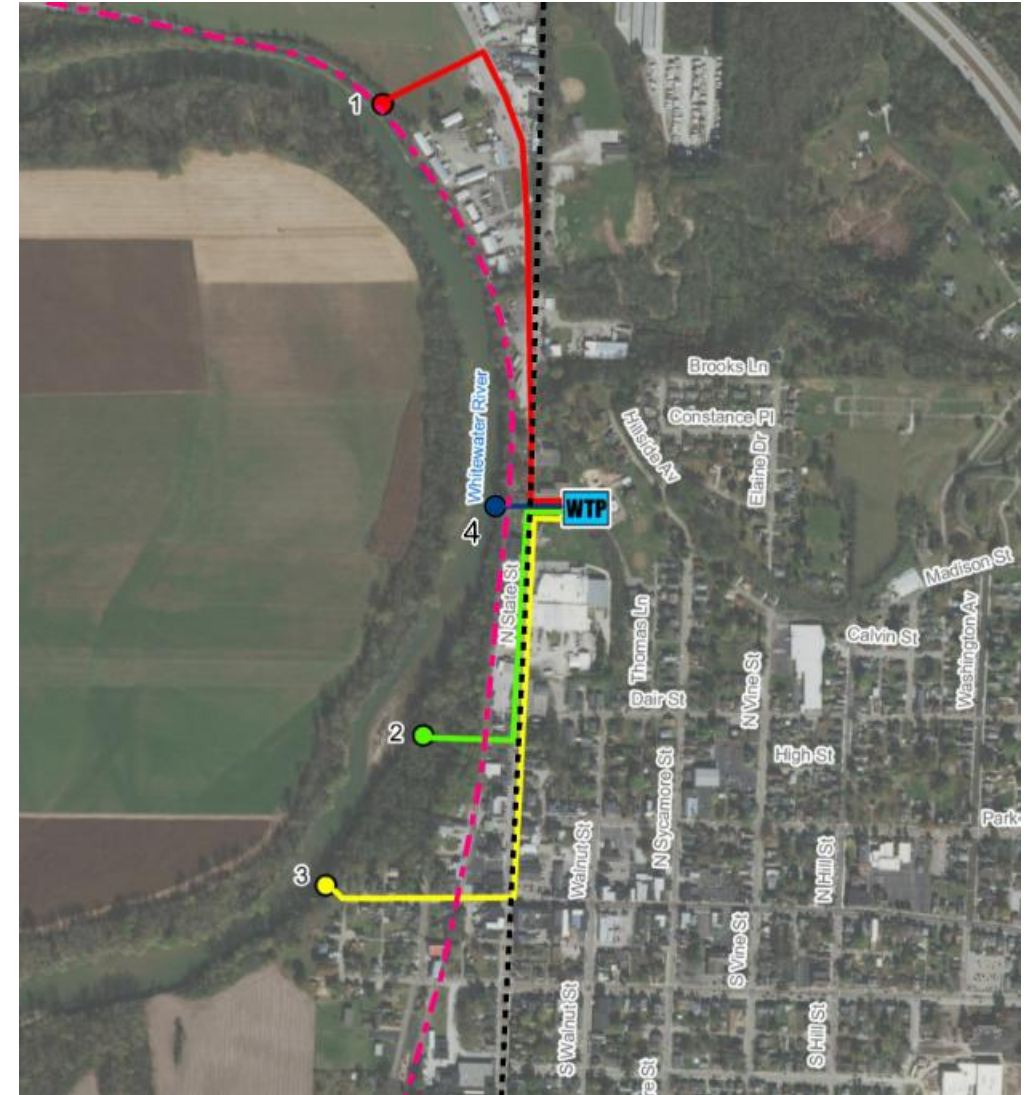
Hydrofluosilicic Acid



Sodium Hypochlorite

Permits

- USACE – Section 401 WQC Regional Permit
 - IDNR
- NPDES
 - Antidegradation application
 - Raw water analysis
- OEPA – Plan approval
- Genesee & Wyoming railroad permit





Genesee & Wyoming Railroad Permit

- Right of way
- Shutoff valves
- Casing pipe
- Minimum separation

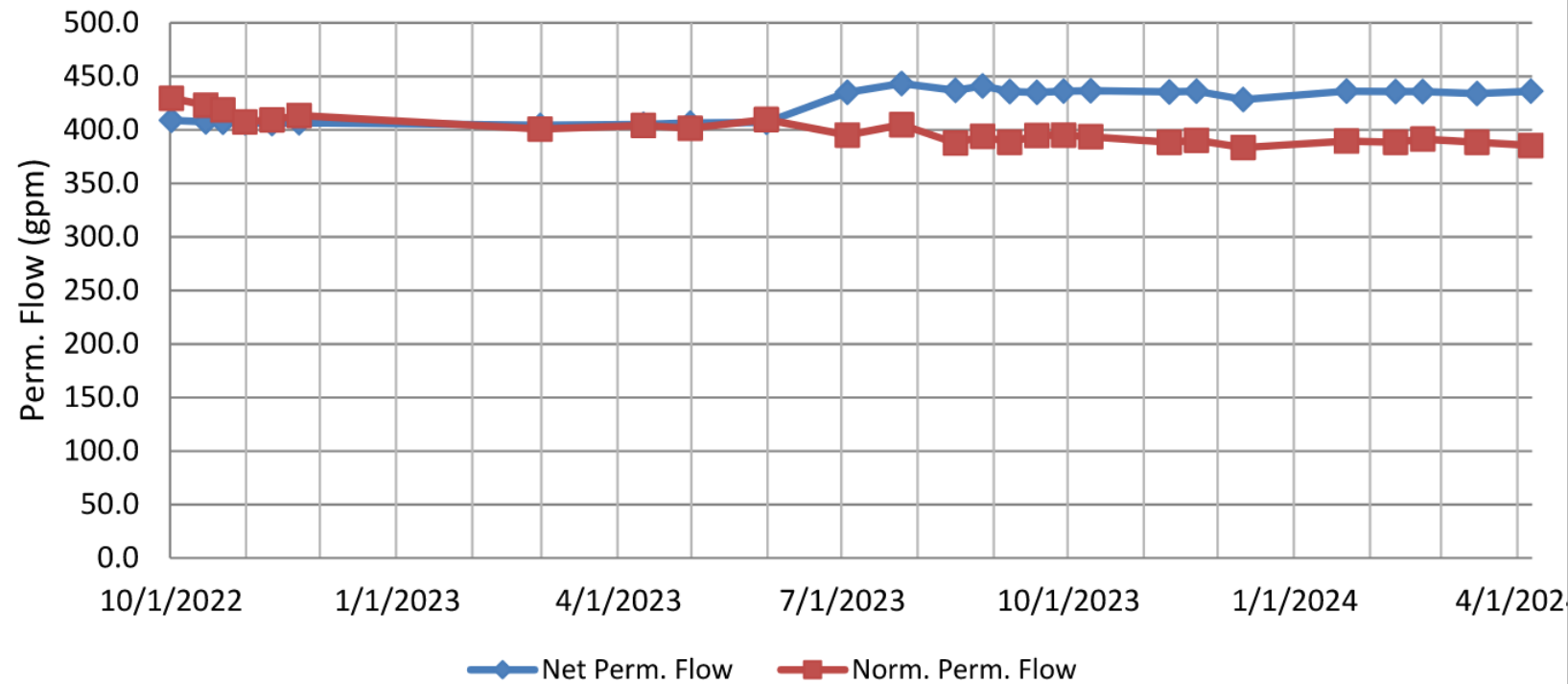


System Performance

- Online for 1 year 8 months
- Skid No. 1
 - 1st CIP performed 11/2023
- Skid No. 2
 - 1st CIP performed 9/2023
- Skid No. 3
 - 1st CIP performed 8/2023
- Cleaning Regiment
 - RoClean L403 and RoClean L211
 - 2% heated solution
- Additional Cleanings
 - Second CIP's 8/2024

System Performance: Flow

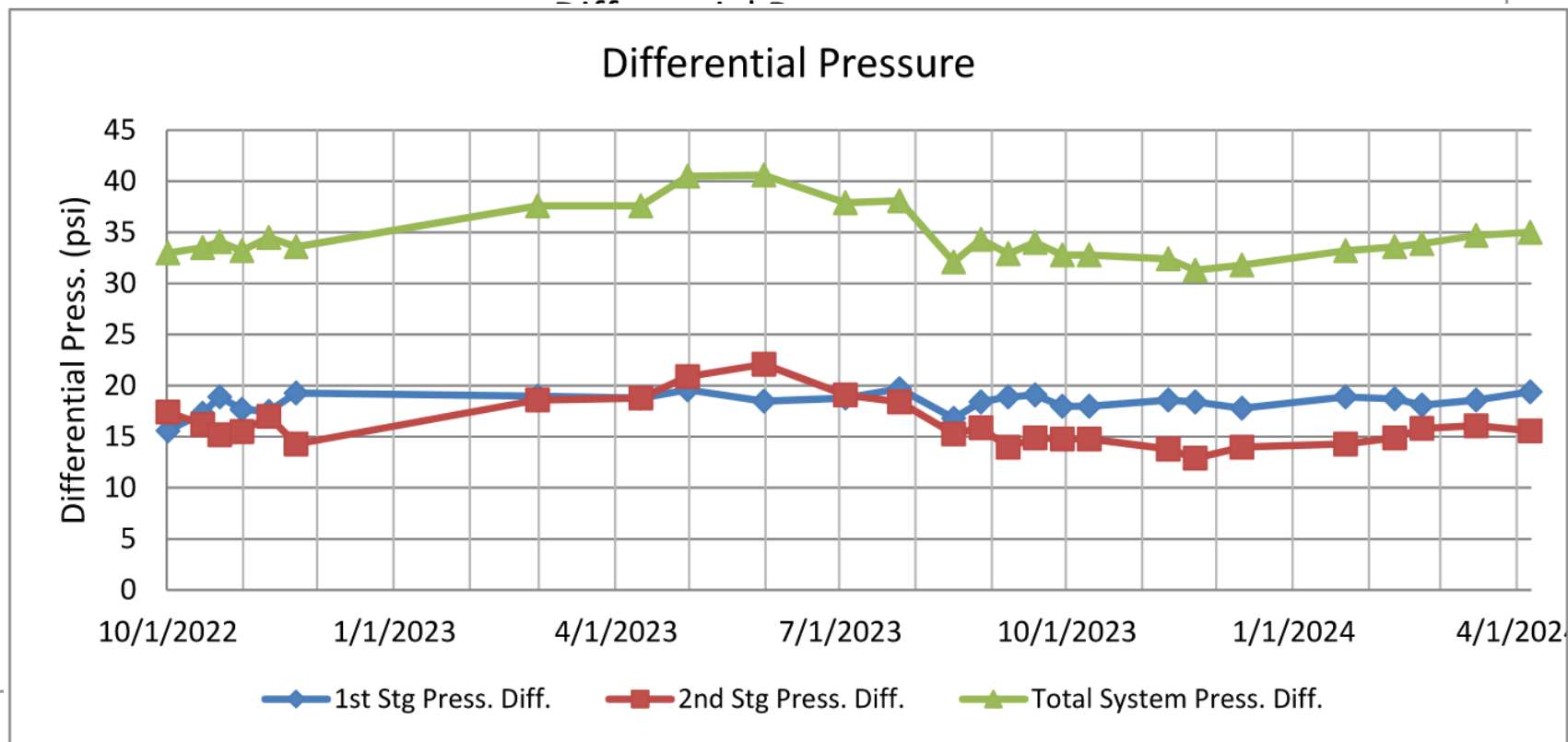
Normalized vs. Net Permeate Flow



Skid No. 3

System
Performance:

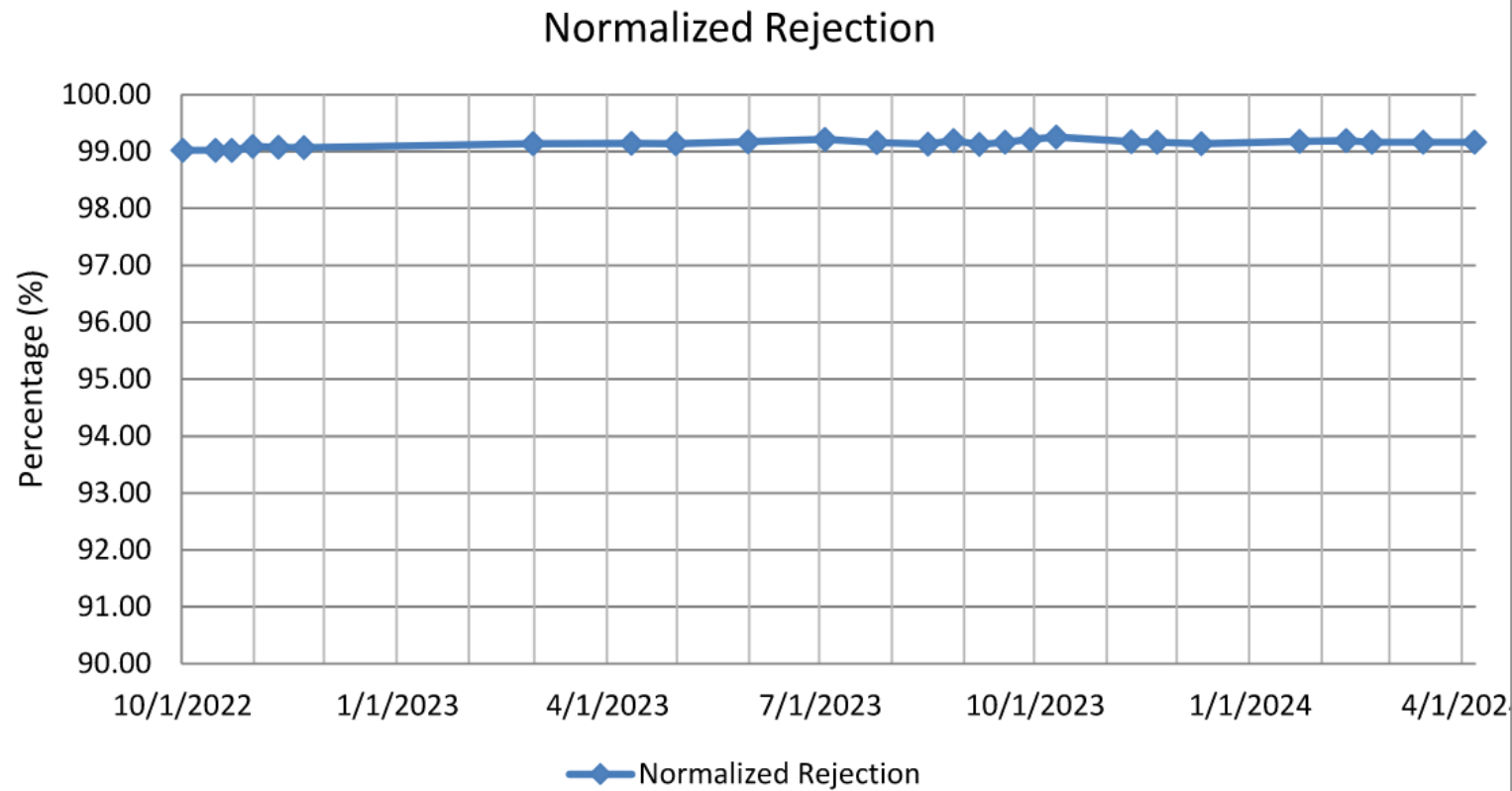
Differential
Pressure



Skid No. 3

System Performance: Rejection

FilmTec BW30XFRLE-400/34i
Minimum Salt Rejection: 99.1%



Skid No. 3

Funding

- **How we are funded**
 - Water Supply Revolving Loan Account (WSRLA)
- **Process to get funded**
 - March 1st for project nominations
 - Design: Application submitted February 2018
 - Conceptual design/general plan for water treatment
 - Basis of design
 - Inorganic raw water analyses for wells
 - Construction: Application submitted February 2019, re-nomination February 2020
 - Capability assurance assessment
- **Interest rate City received**
 - Design – 0% over 5 years, \$700,000
 - Construction – 0.53% over 20 years, \$6,689,000



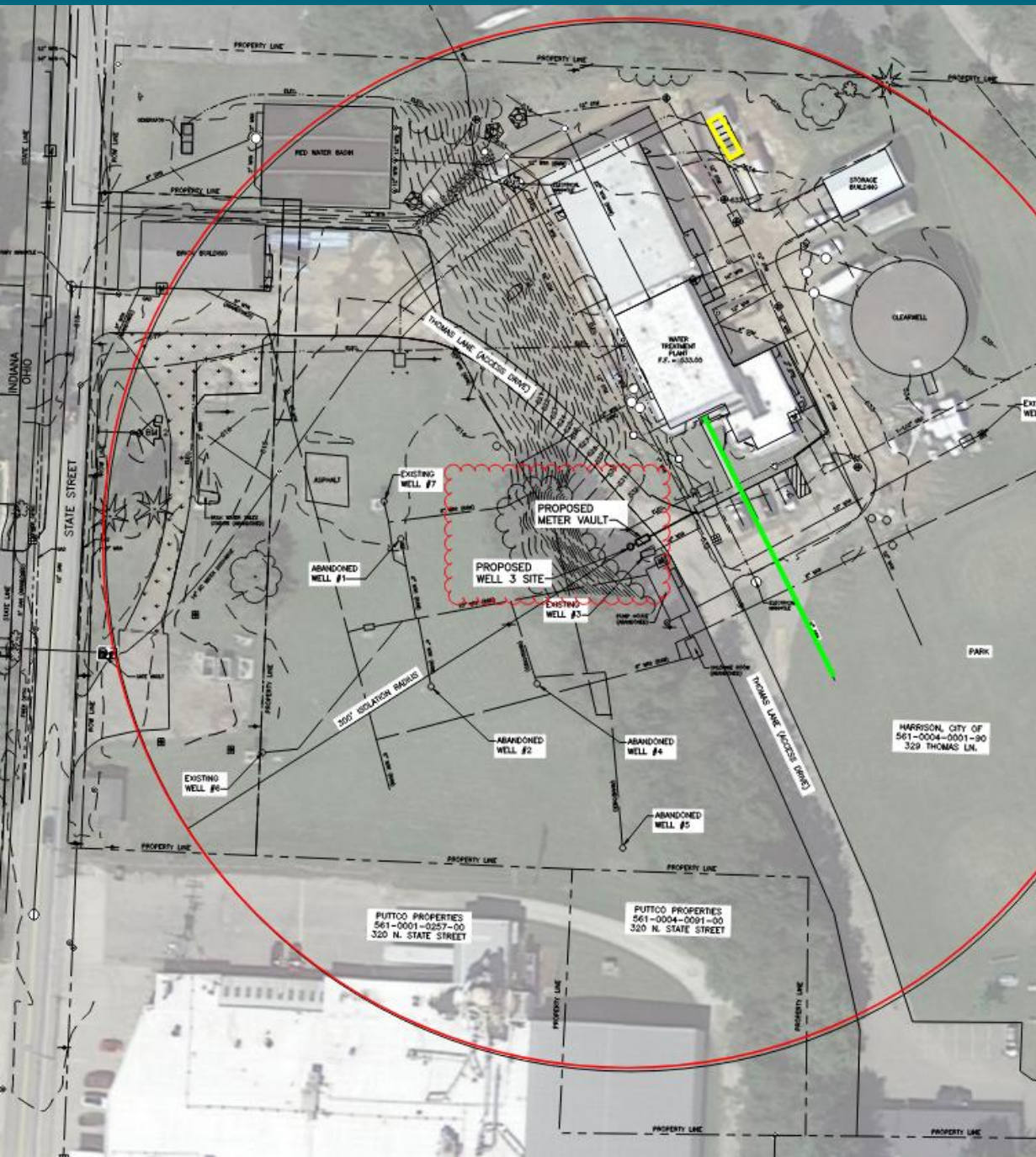
Water Supply Expansion

Prior Water Supply:
Four Ohio Wells: 3,5,7 & 8
Two Indiana Wells: 1 & 2

Ohio Well No. 3

- Originally installed in 1973
- Declining production
- Rehabilitation and lining considered
- Isolation radius considerations
- OEPA not receptive to issuing a variance for a new well

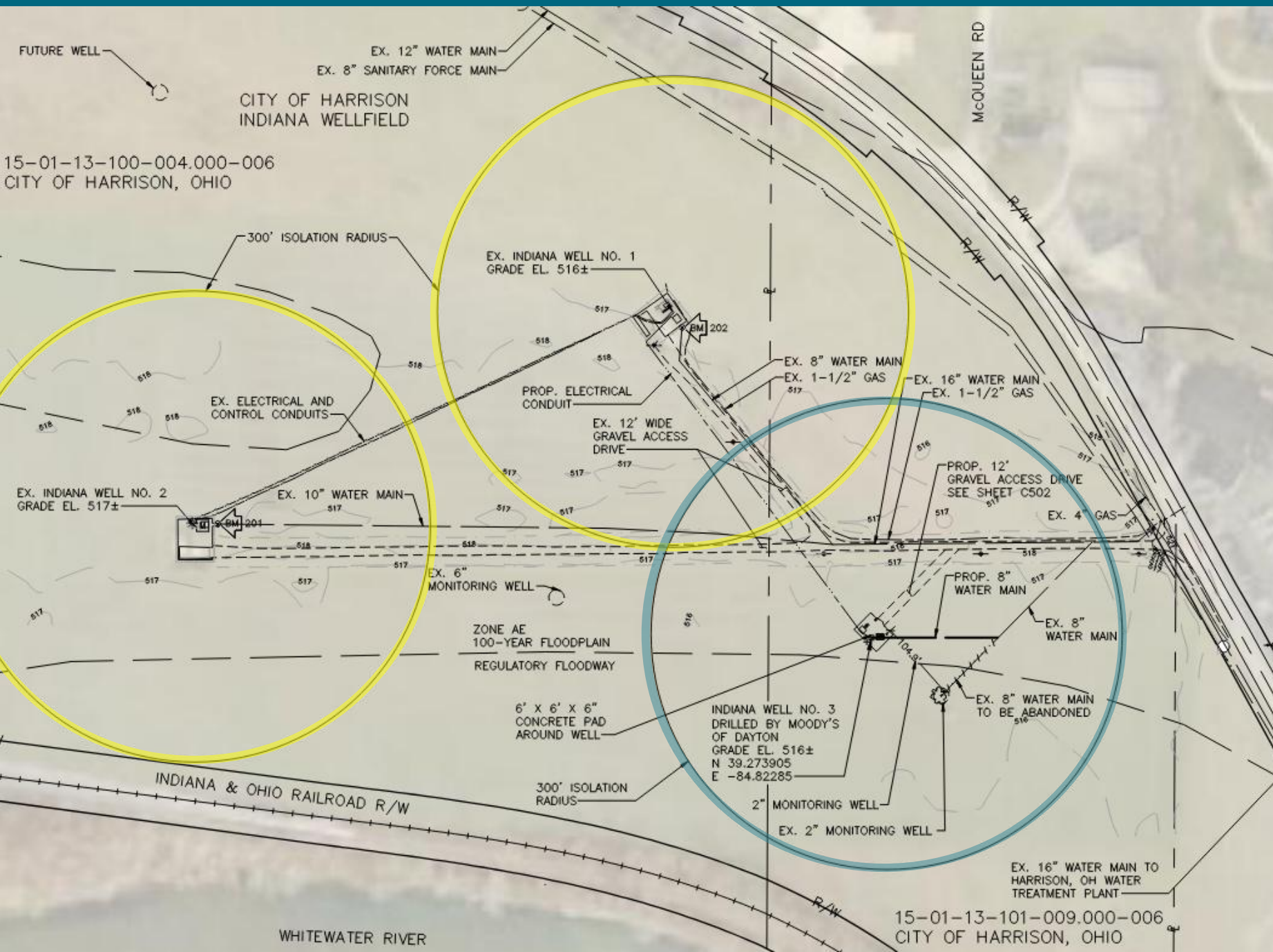




Ohio Well No. 3

Multiple potential sources of contamination within the 300-foot isolation radius

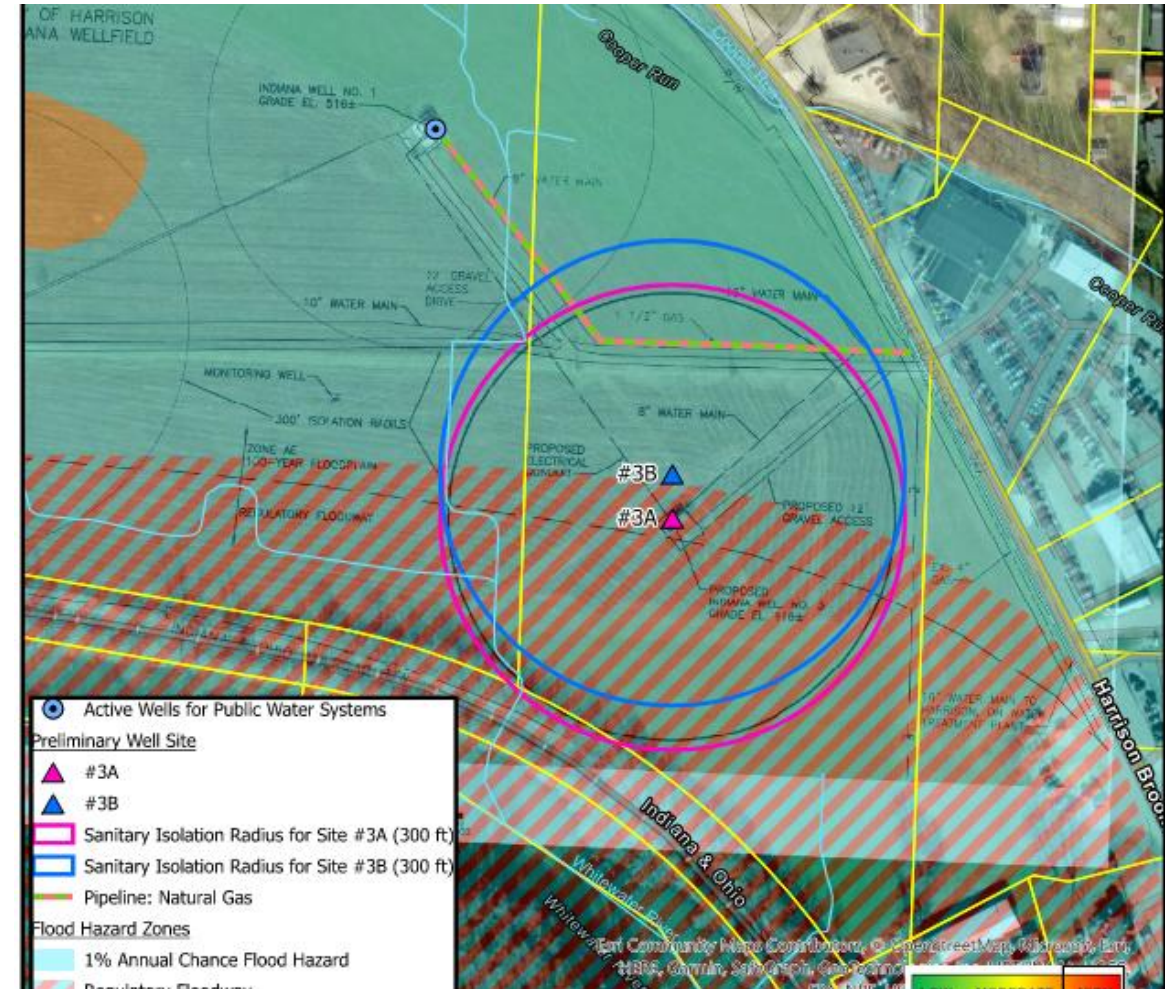
- Sanitary sewer lateral serving the plant
- Emergency generator with diesel fuel storage tank
- Chemicals for water treatment
- Industrial property to the southwest



Indiana Wellfield

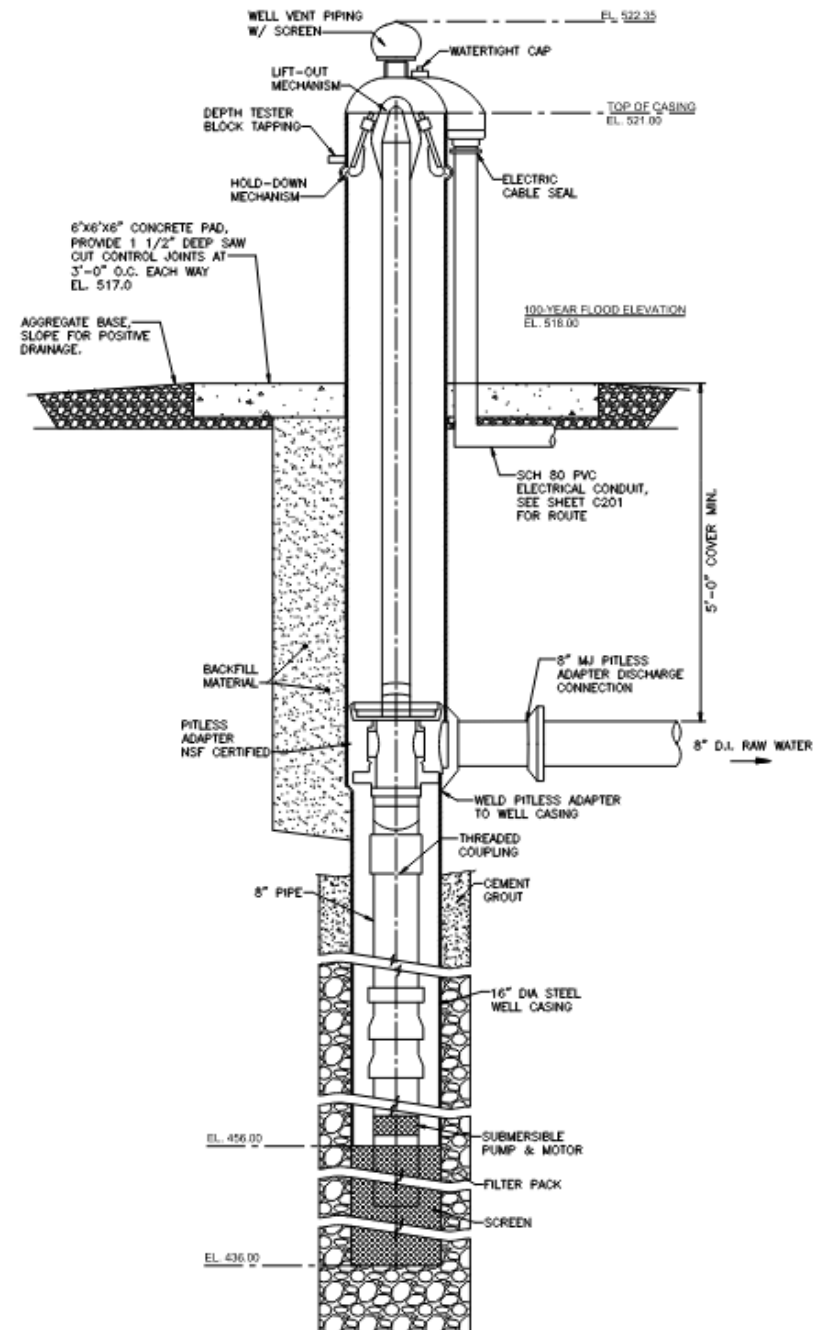
Indiana Wellfield

- Well No. 3 planned for the southeast corner
- Location shifted north to avoid the floodway of the Whitewater River and a lightly used railroad line
- Also avoided the road and a sanitary force main to the northeast
- Isolation radius contained within City property

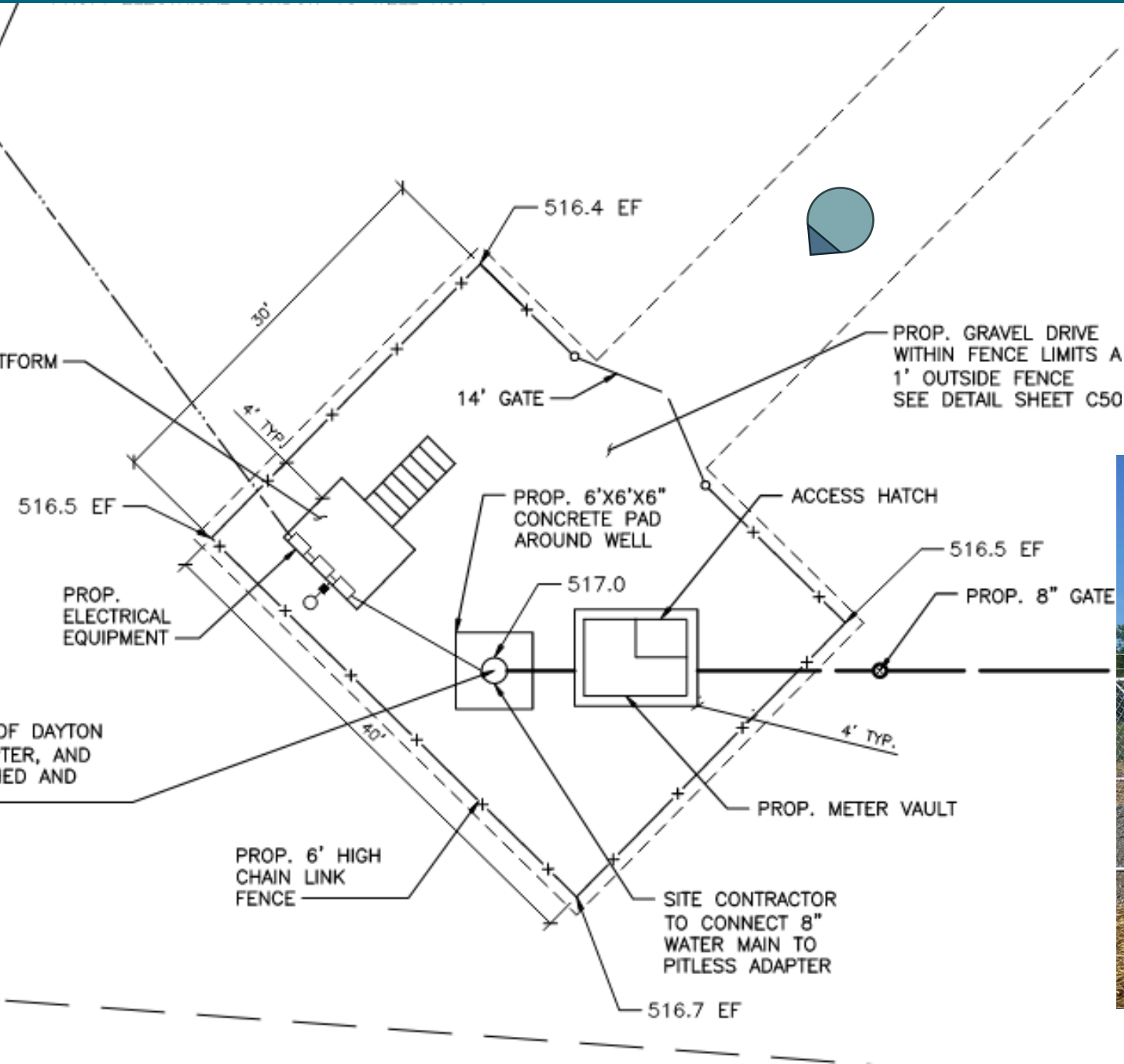


Well Profile

- Provided for OEPA permit submittal
- Filter pack provided around the well screen
- Annular space grouted
- Pitless adapter
- Surrounding grade sloped away from the well
- Top of casing required to be at least three feet above the flood elevation



Well Profile





Thank You

City of Harrison:

*Jim Leslie,
Public Works Director*

*Terry Knueven,
Water Superintendent*

General Contractor:

Building Crafts

Contact Information:

*Brian Phillips
bdphillips@fishbeck.com*

Thank You

